

ADVANCED RED LEAD USED in BATTERY FORMATION – IMPACT on COSTS, BATTERY LIFE, and ENVIRONMENTAL FOOTPRINT

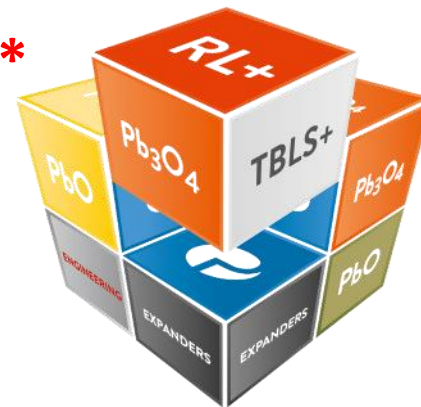
Rainer Bußar, Hamid Ramianpour, Micha Kirchgeßner, PENOX GmbH (D)

FENIBAT Conference, Londrina, Brazil

(Version V4 – dated 04.10.2023)



- Basics & Introduction
- Formation study* with different types of PENOX Red Lead
- Carbon Dioxide (CO₂) Mitigation, Process Time Reduction
- Findings & Summary
- **“Functional Red Lead” = Red Lead Plus (RL+)****



* First part of the formation study was presented on ELBC 2022

** RL+ was first presented to the battery industry at the FENIBAT 2022



- Process duration
10 to 20 h (flooded technology)
>20 to 30 h (AGM technology)
- Formation charge (Ah based related to PAM)
300 to 600 Ah/kg (flooded)
400 to 500 Ah/kg (AGM Technology)
- **Formation energy (Wh based related to PAM)**
660 to 1300 Wh/kg in a **2V cell**
4.0 to 7.8 kWh/kg in a **12V battery**
- *Formation factor*
3 to 6 depending on technology
- **Energy costs**
driven by formation efficiency
- **Process costs**
balanced time vs. efficiency

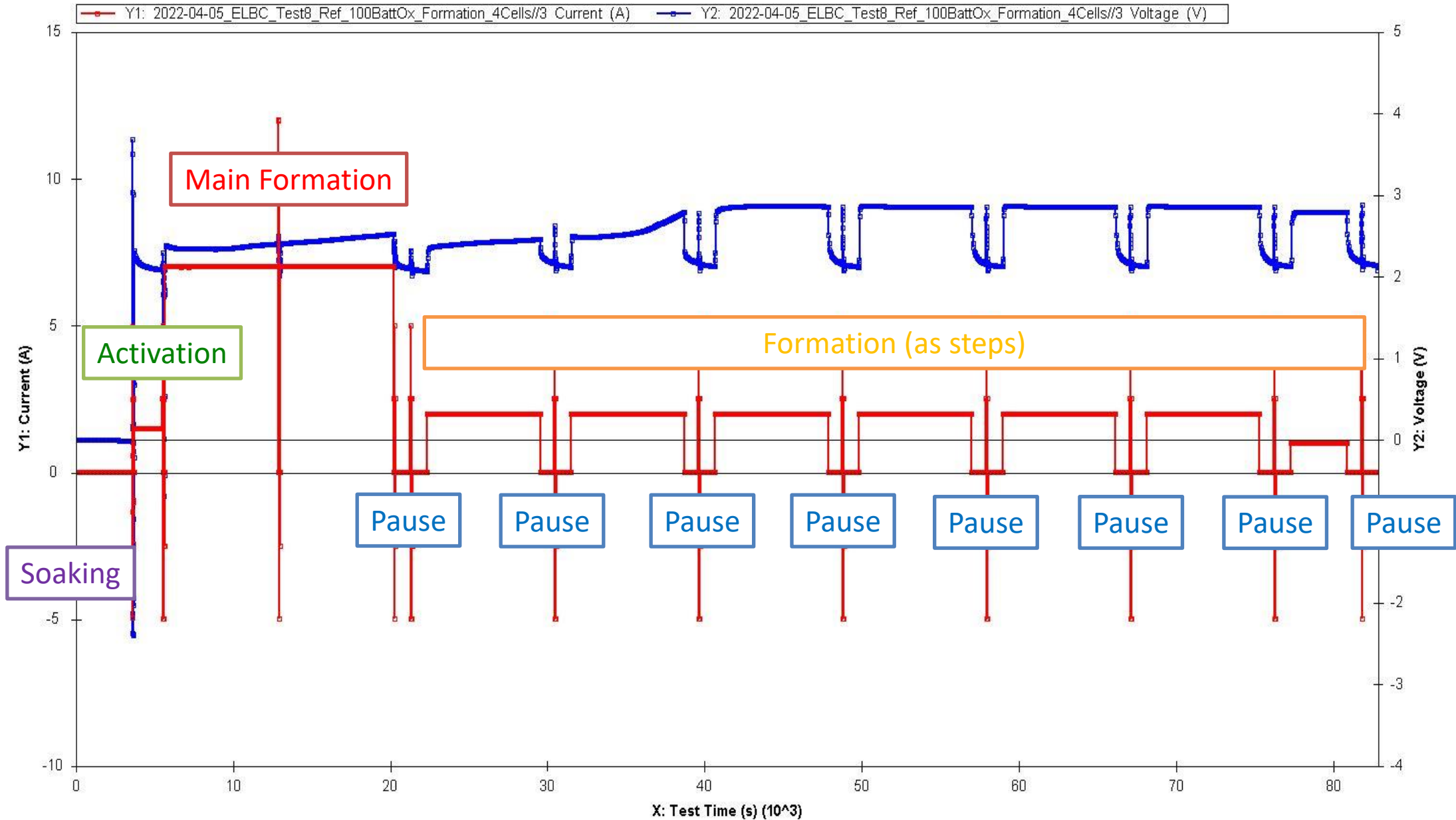
The Formation process can be optimized by tuning the key-factors relevant for an effective transformation of the electrical energy into chemical energy in both electrode polarities.

A basic conflict is typically the demand for a fast process and a high energy efficiency

Typical Formation Steps (Flooded Technology*): “two-shot formation” => PENOX Reference Study

- **Soaking of the cell**
 - Depending on plate thickness and electrolyte density max. 1 h – optimum often with 0.5 h
- **Activation Step**
 - Low current density to create a basic conductivity
 - Typical duration 0.5 to 1h with a current of 0.1 to 0.3 A per Ah
- **Main formation Step with high current**
 - High current step with 0.5 to 1 A per Ah – time is limited by the charge acceptance of the NAM
 - Step must be ended before the negative plates show a high over-potential
- **Pause before following steps with reduced current density**
 - Typical rest time is 15 minutes to 0.5h depending on plate thickness to allow electrolyte migration and degassing
- **Formation Steps with reduced current**
 - Typically several steps with reduced current are following

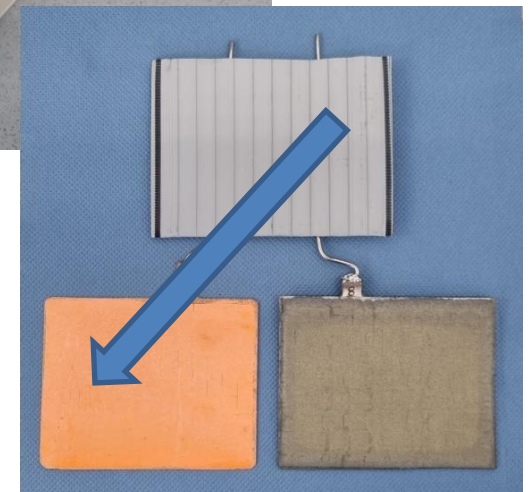
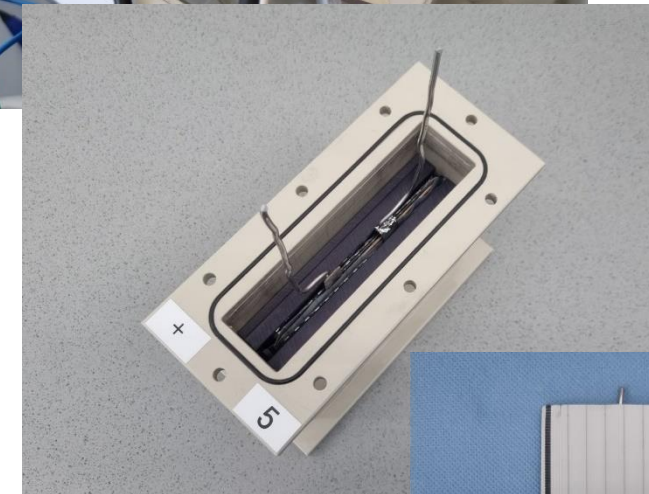
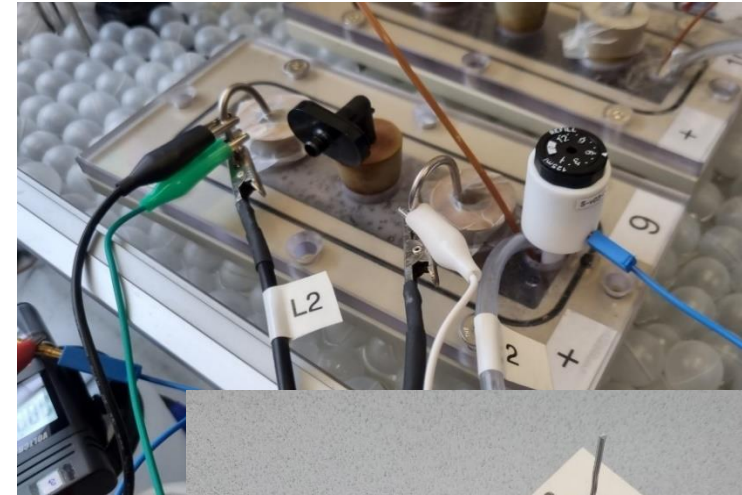
*This profile is based on a flooded cell – in our study we have used 1p / 2n set-up, Electrolyte density is 1.15 g/cm³.



- General Comments on AGM:
 - AGM formation runs much longer – current limitations and pauses in formation are important
 - The formation requires to allow for a specific water loss, to reach the target acid density
 - Control of the plate process, to control the electrolyte contained within the active mass is crucial
 - PENOX believes that Red Lead (RL) is mandatory in PAM to achieve optimal performance for AGM technology
- Investigations:
 - PENOX has studied first the effect of RL in a simplified flooded set-up
 - The impact of the structure of the PAM was investigated (still on-going)
 - However, it became clear that the NAM structure is very relevant as well (new study started)
 - Future updates concerning AGM technology will be posted under: https://penoxgroup.com/AGM_news

- Systematic testing of PAM mixes with:
 - We used industrial **Red lead (RL)** with d50 4.5 μm and PbO_2 (lead dioxide) 25 to 27%
 - Different contents of **Red lead (RL)** 0%, 10%, 25%, 50%, 75% and 100%
 - Comparison of **tri-basic (3BS)** and **tetra-basic (4BS)** cured positive active masses (PAM)
- Conditions of the RL study:
 - Same formation profile was used, only duration was varied to change the formation factor
 - Formation factor was systematically varied, and the resulting lead dioxide (PbO_2) content analysed
 - Structural investigation of the cured plates (of the formed plates)
 - Testing of initial C20 / C5 capacity and initial capacity evolution
 - Impact of the negative plate was investigated using reference electrodes

- Cell Set-up:
 - Grid technology is gravity cast grids
 - One positive plate (1p) with C20: 12 Ah nominal
 - Two negative plates (2n)
 - PAM : NAM ratio in weight equals: 1 : 1.8*
 - Electrolyte: 300 g, density 1.28 +/- 0.05 g/cm³
 - C20, **C5** was tested at 20 to 22 °C
- Variation of the reference:
 - M-neg. plate is a ***standard negative***
 - J-neg. plate is a ***negative plate with advanced carbon***



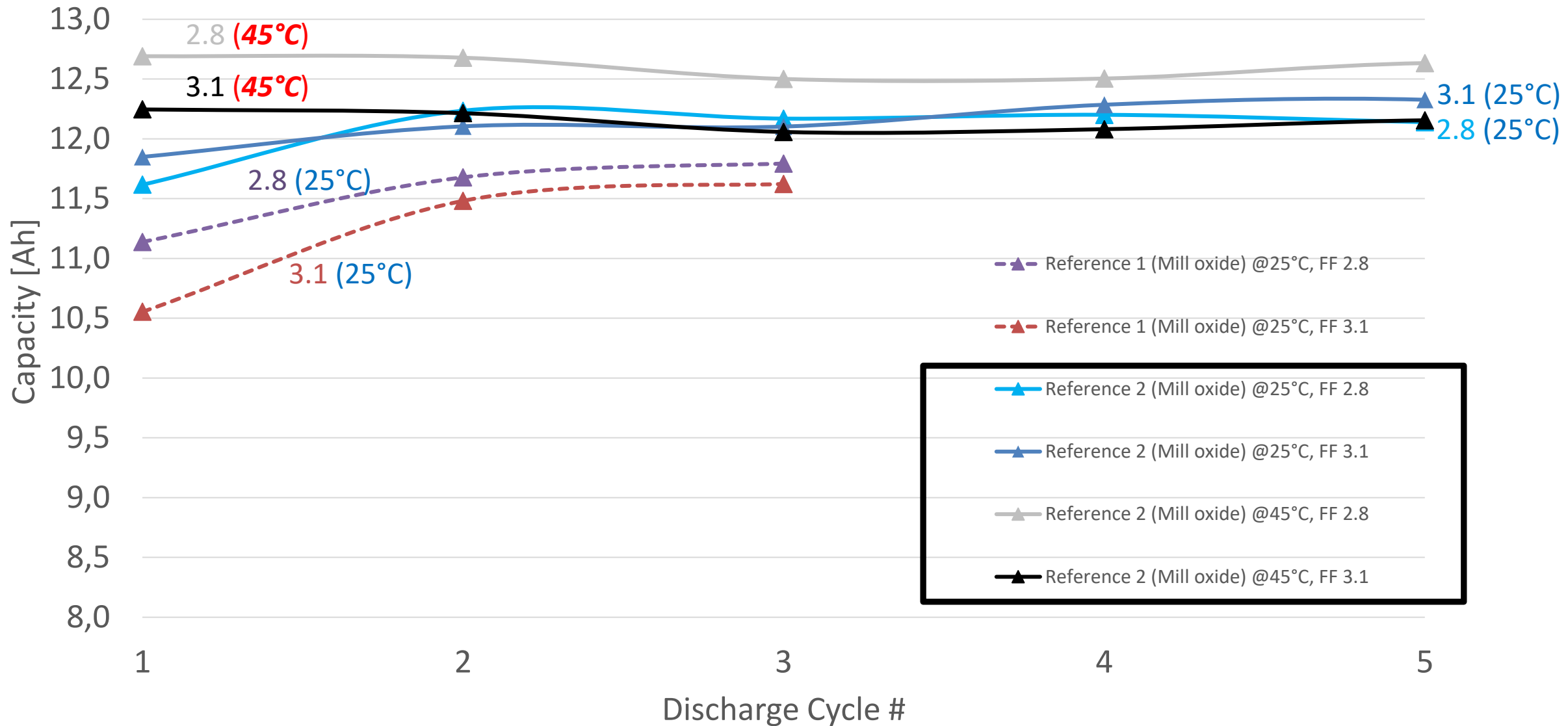
*This high NAM content is reducing the impact of the NAM, as this study is focussing on PAM. PENOX will compare the identified optimal PAM in a normal battery design, e.g. (5p/4n).

Industrial Plate based Reference Systems	Cell Set-up	Structure	H2O Poro	Formation Factor	PbO2 Content (%)		Average Target: 85 +/- 3 %
					upper %	lower %	
Reference 1 (Mill oxide) @25°C	1p2n - M neg.*	3BS	40	2.8	72.4	69.6	71.0
				3.1	72.0	70.6	71.3
Reference 1 (Mill oxide) @35°C	1p2n - M neg.	3BS	40	2.8	82.3	80.4	81.4
				3.1	83.0	81.6	82.3
Reference 1 (Mill oxide) @45°C	1p2n - M neg.	3BS	40	2.8	85.4	83.0	84.2
				3.1	91.6	84.4	88.0
Reference 2 (Mill oxide) @25°C	1p2n - J neg.**	3BS	40	2.8	74.4	69.2	71.8
				3.1	72.0	70.0	71.0
Reference 2 (Mill oxide) @35°C	1p2n - J neg.	3BS	40	2.8	81.2	77.5	79.4
				3.1	81.3	78.2	79.8
Reference 2 (Mill oxide) @45°C	1p2n - J neg.	3BS	40	2.8	87.1	81.8	84.5
				3.1	87.3	84.7	86.0
References produced in PENOX laboratory							
PENOX Reference 3 (100% Battox PAM) @45°C	1p2n - J neg.	3BS	50	2.8	69.8	71.3	70.6
				3.7	84.0	84.0	84.0

* M-neg. plate is a *standard negative (SLI)*; **J-neg. plate is a *negative plate with advanced carbon (EFB type)*

- Formation of the **reference cells** required a formation factor of **3.1 up to 3.7**
- Formation of the **reference cells** required about **420 to 500 Ah per kg** of PAM
- Temperature of **25°C** is too low for an effective formation
- **Temperature of 45°C** allows a fast formation
- Evolution of the C5 capacities are shown on the next slide – *please note that for the industrial reference plates we can not know the individual PAM weight – plate weight was measured.*

C5 Capacities from Reference Cells – all positive Plates are formed from 3BS cured plates



For the reference plates only the total plate weights known

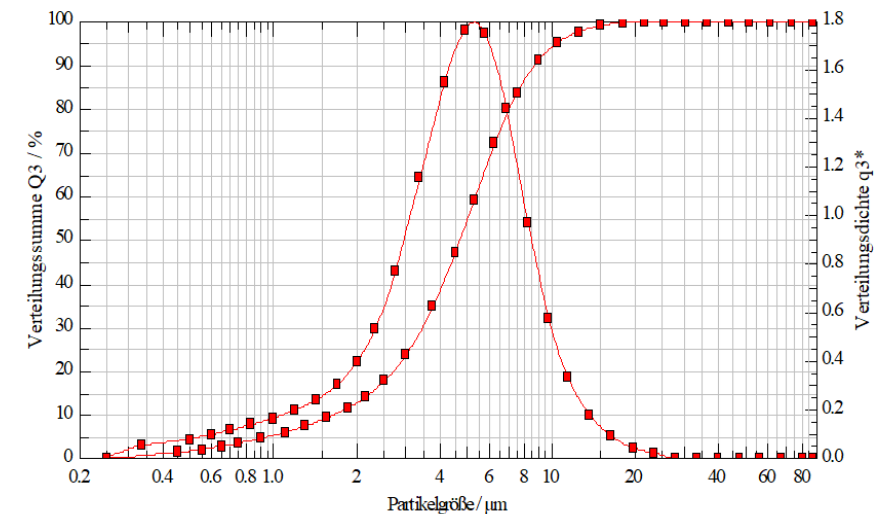
RL+ is an „advanced Red Lead (RL):

- It is free flowing powder similar to normal red lead.
- The particle size distribution (PSD) curve follows the PSD-curve of the standard red lead
- **The surface is coated with tetrabasic seeding crystals.**

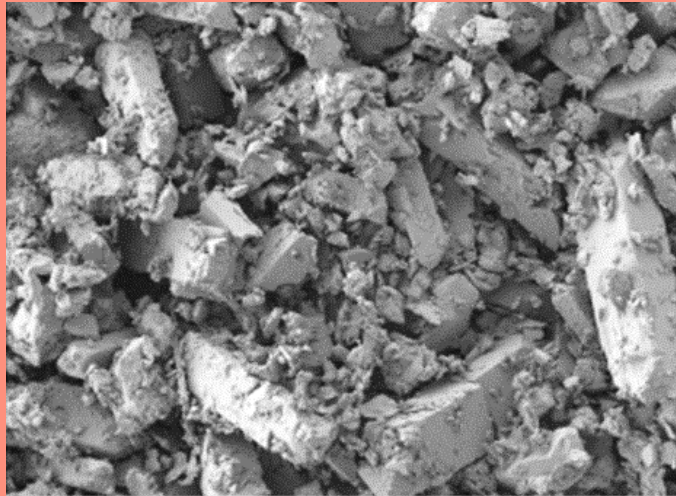
RL+ can be produced by PENOX from different types of Pb_3O_4 . However, PENOX recommends to use standard industrial grades of RL.

RL+ is available as a standard product with a 4BS content of 1.5 w%.

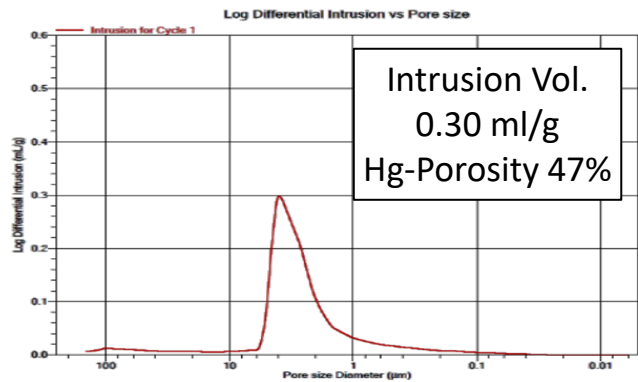
- Depending on demand different loadings can be produced and made available, up to 5 w% 4BS.



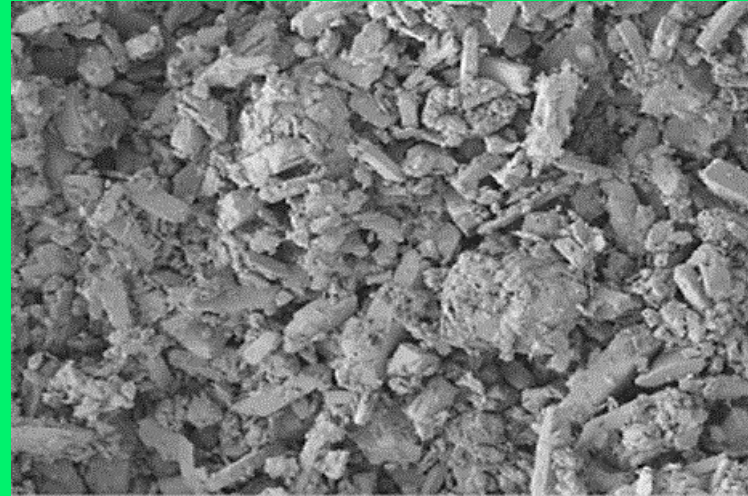
0.5% Powder 4BS seeds



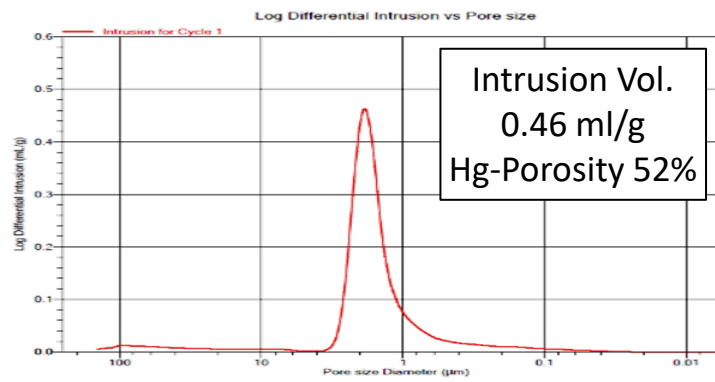
00277003 5 μm ChemiLytics



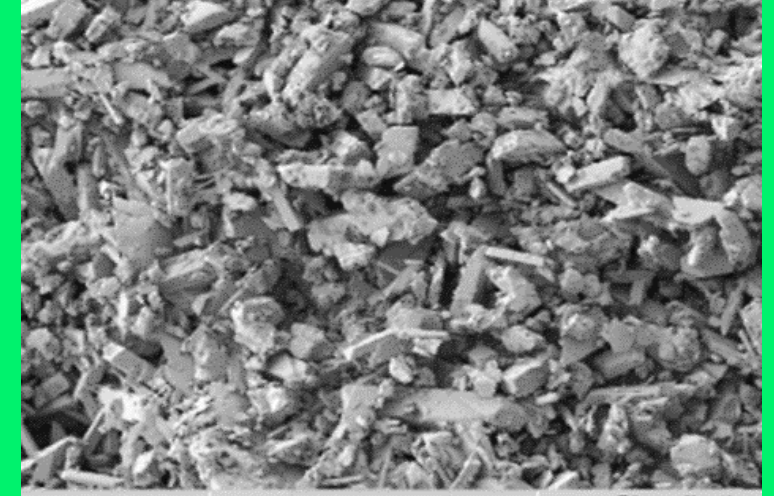
TBLS+[®] with 0.5%¹ 4BS seeds



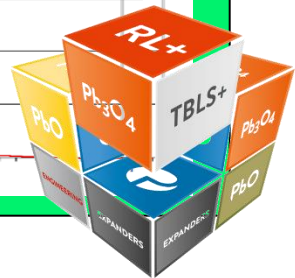
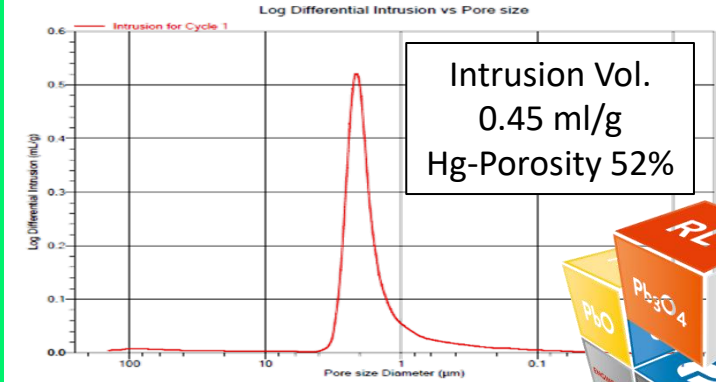
00277007 5 μm ChemiLytics



RL+ with 0.5% 4BS seeds



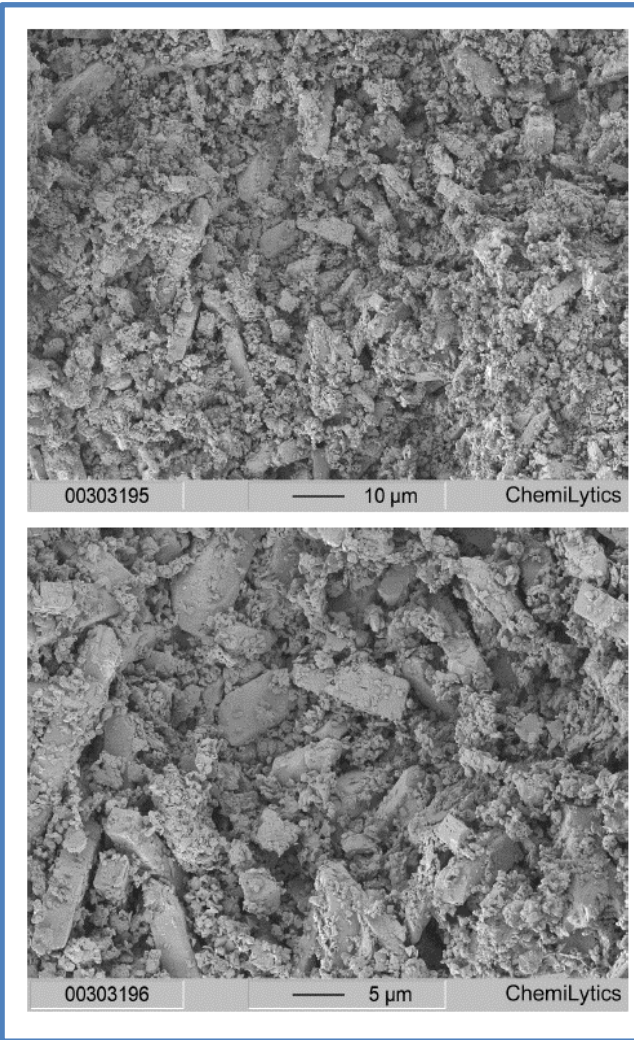
00276999 5 μm ChemiLytics



- Coarse (powder based) seeds result in larger 4BS crystals after curing
- TBLS+[®] contains fine seed crystals with d50 of 0.5 to 0.7 μm, which results in the growth of smaller 4BS crystals
- **RL+ is coated with similar fine 4BS seed crystals, which result in an identical 4BS crystal growth**

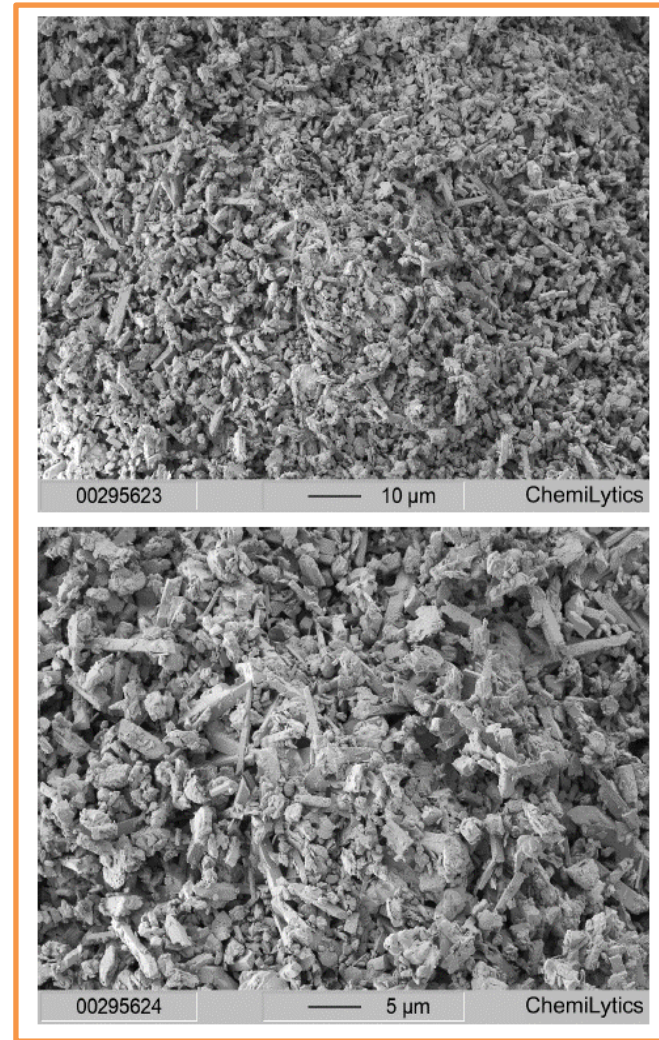


0.15% 4BS seeds



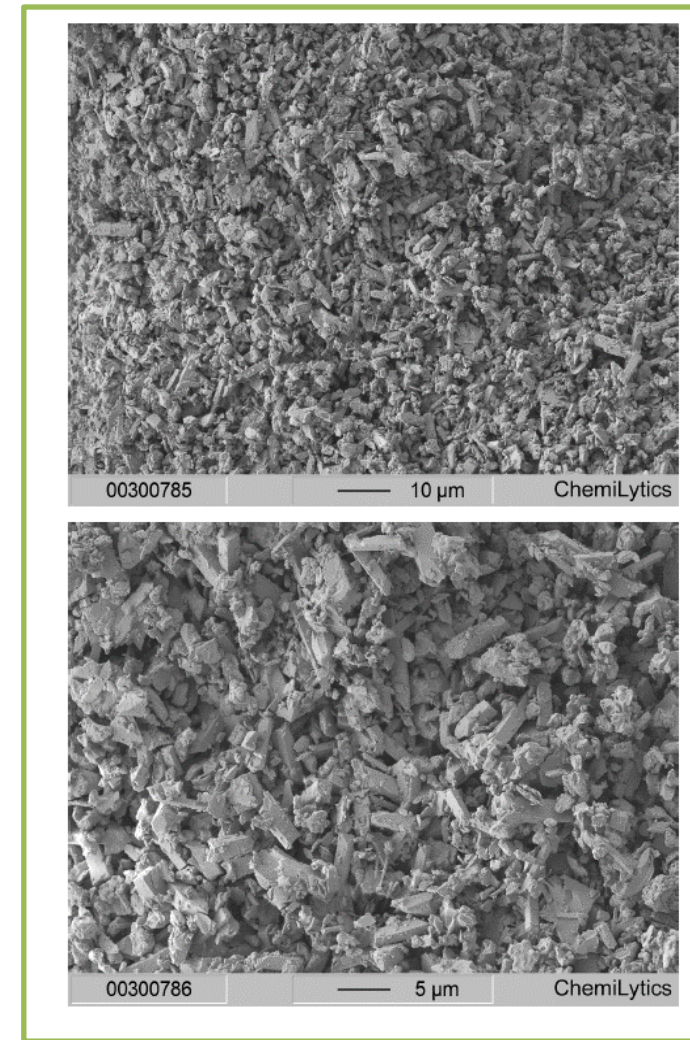
Battery Oxide weight%	Red Lead weight%
90%	10% RL+

0.38% 4BS seeds



Battery Oxide weight%	Red Lead weight%
75%	25% RL+

0.38% 4BS seeds



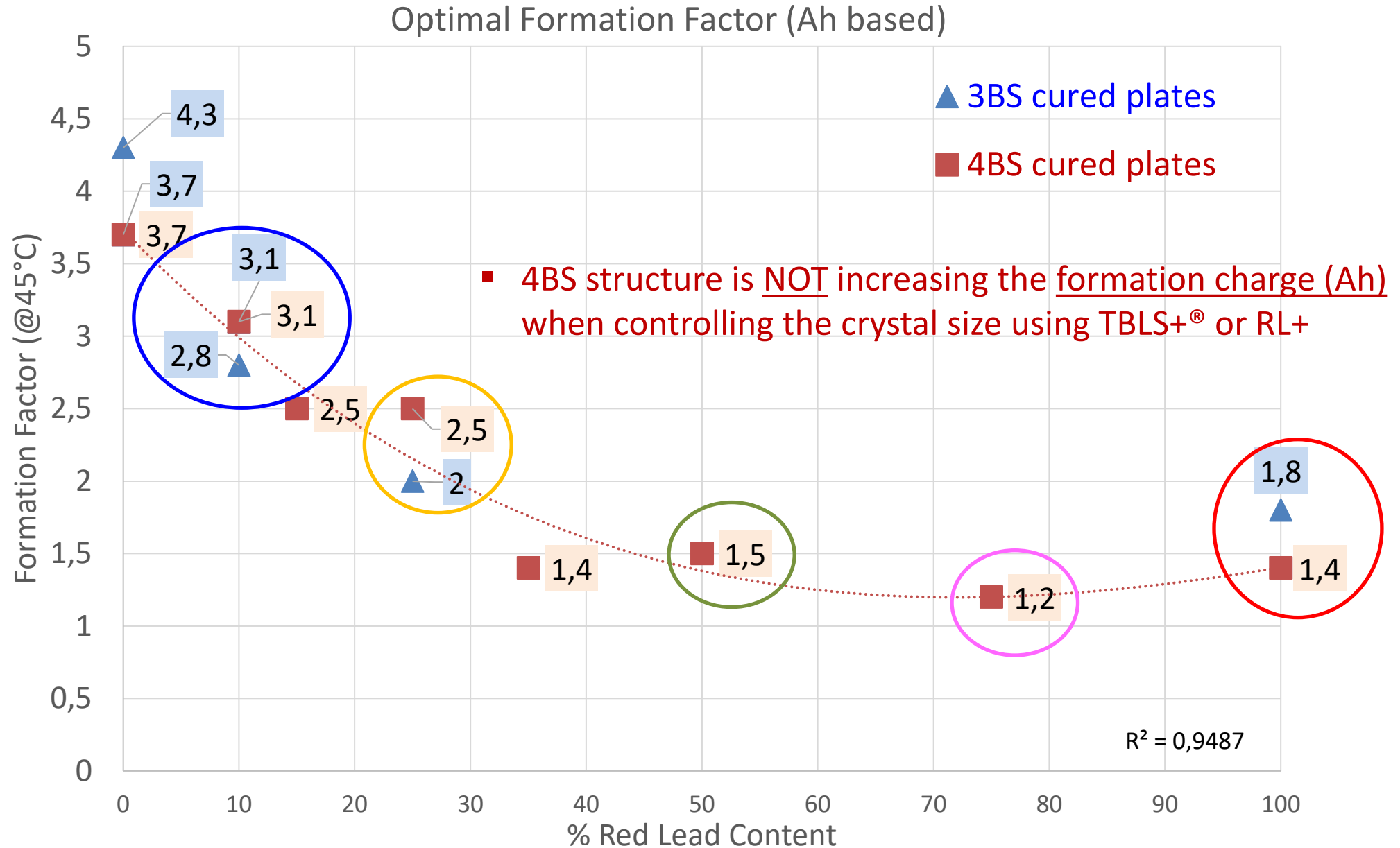
Battery Oxide weight%	Red Lead weight%
50%	25% RL+ & 25% RL

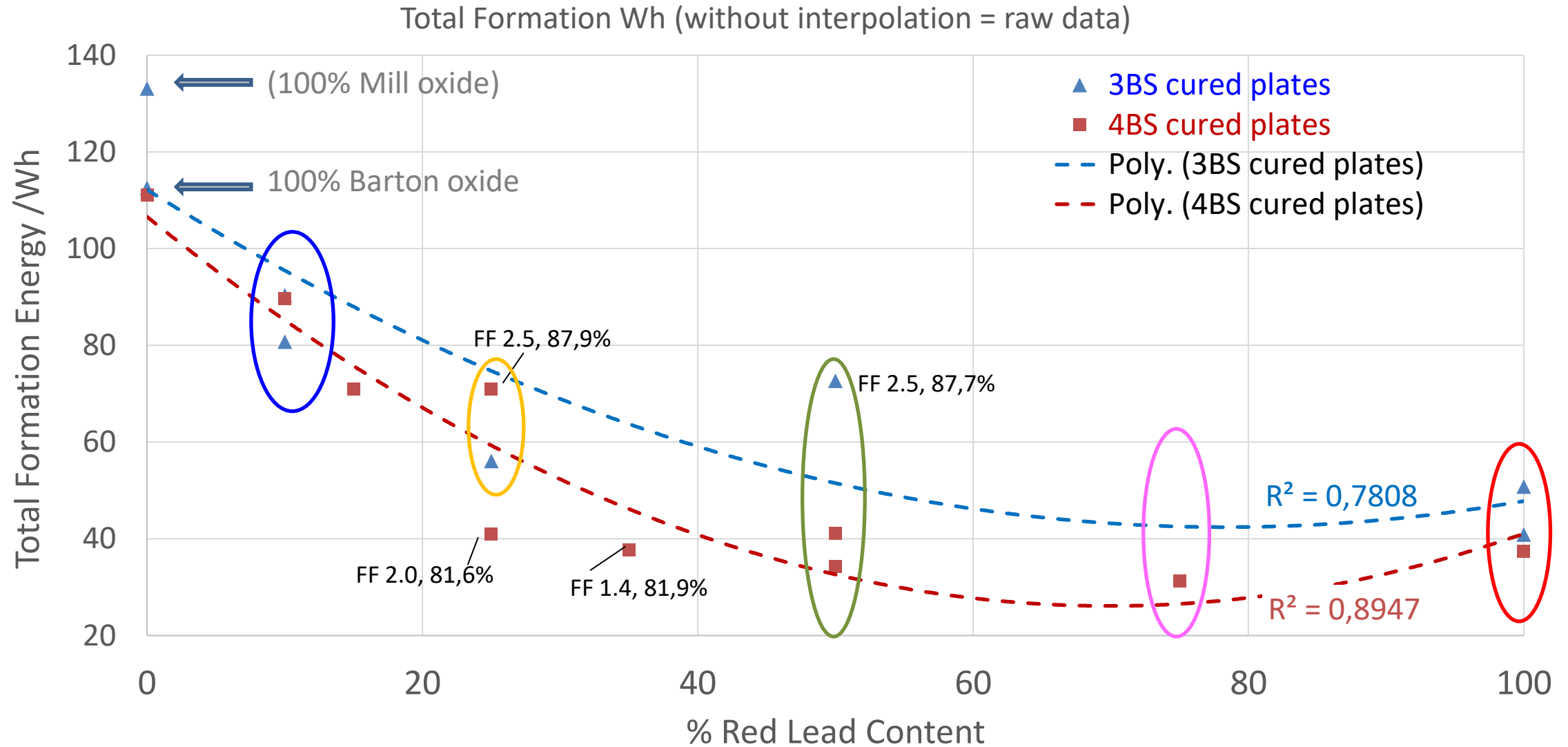
Impact of RL-Content – 4BS Structure

PAM composition		PAM Structure	H2O Porosity	Formation Factor (FF)	Average PbO2
Battery Oxide weight%	Red Lead weight%	Av. 4BS content	%	(lower is better)	Target: 85 +/- 3 %
100% (Mill oxide)	0%	N/D	N/D	N/D	N/D
100% (Barton oxide)	0% RL+ (*1% TBLS+)	92.6%	49%	3.7	82.3
90%	10%	90.4%	48%	3.1	85.0
85%	15%	93.4%	52%	2.5	85.0
75%	25%	92.6%	59%	2.5	87.9
75%	25%	92.6%	59%	1.5	80.9
65%	35%	80.9%	50%	1.4	81.9
50%	50%	92.1%	49%	1.3	80.2
50%	50%	92.1%	49%	1.5	88.4
25%	75%	84.3%	51%	1.2	85.7
0%	100%	91.6%	46%	1.4	84.1

- * 4BS structure is based on 1% of TBLS+ (0.42% of 4BS seeds in PAM) – Reference formation factor is 3.7
- Formation factor can be reduced to about 2 for 25% of RL+**
- Formation factor can be reduced to about 1.5 for 50% RL (25% of RL and 25% of RL+)

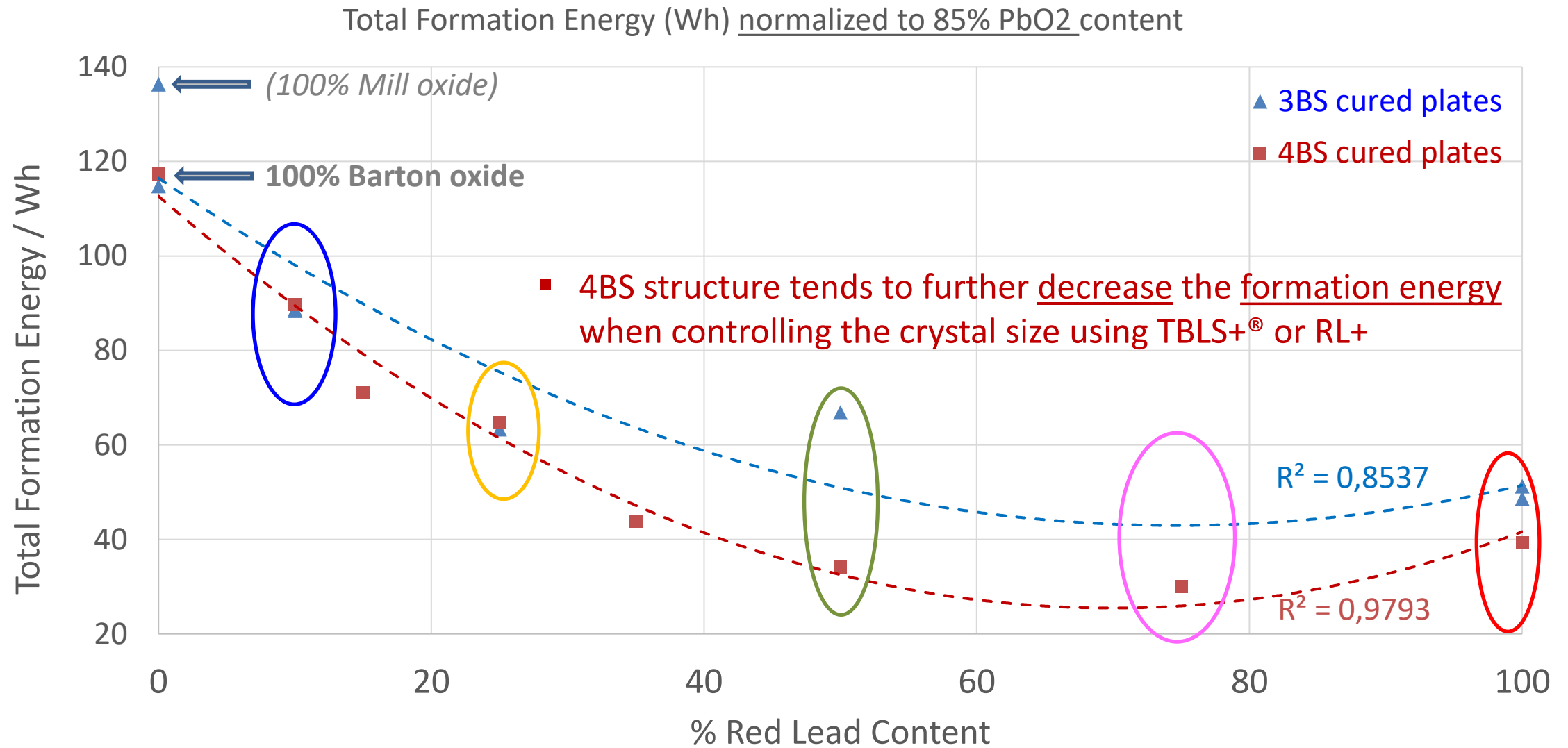
PENOX Formation Factor depending on RL content





* This data-set requires additional measurements to allow for a better fitting.

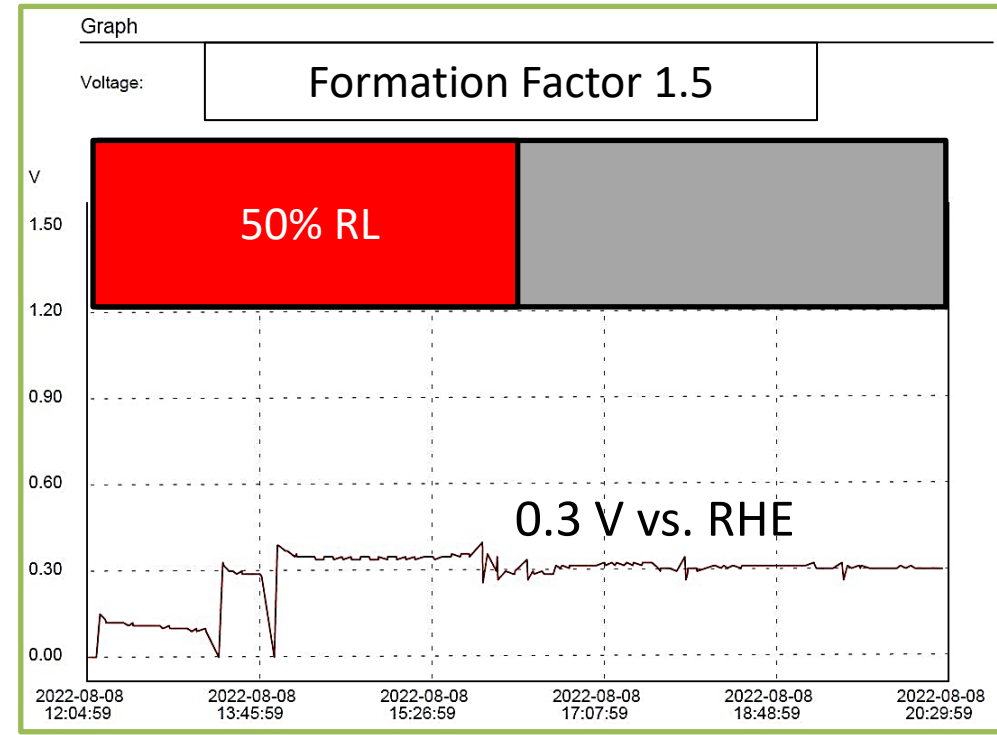
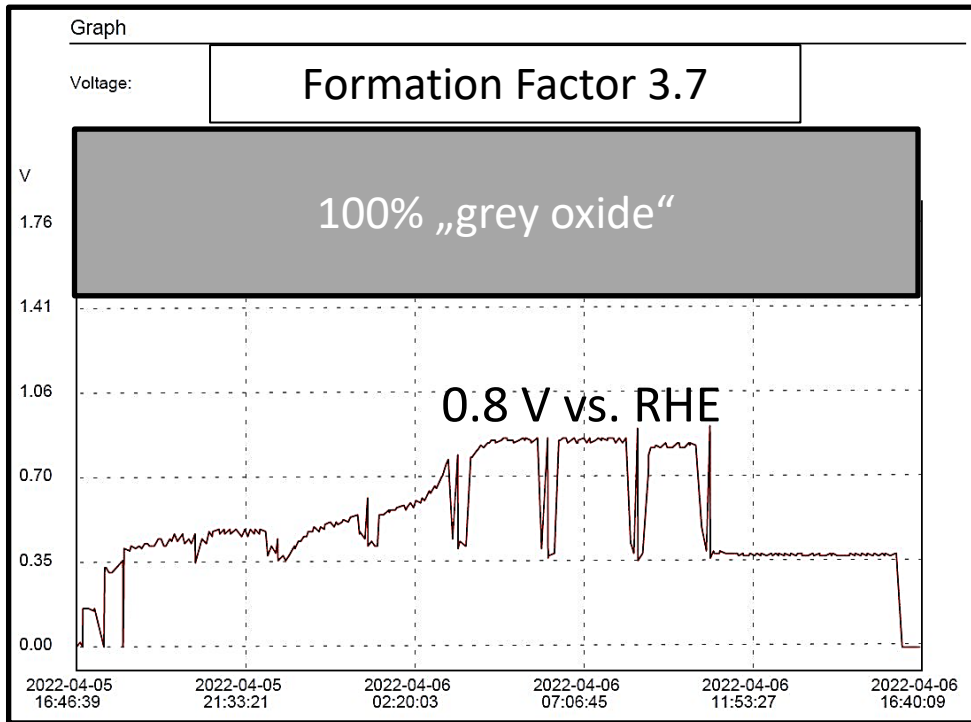
PENOX Formation Energy (Wh based - normalized)



* The formation energy was interpolated to reach 85% of lead dioxide in the PAM.

This interpolation of the **3BS structure** will require further refinement based on additional data.

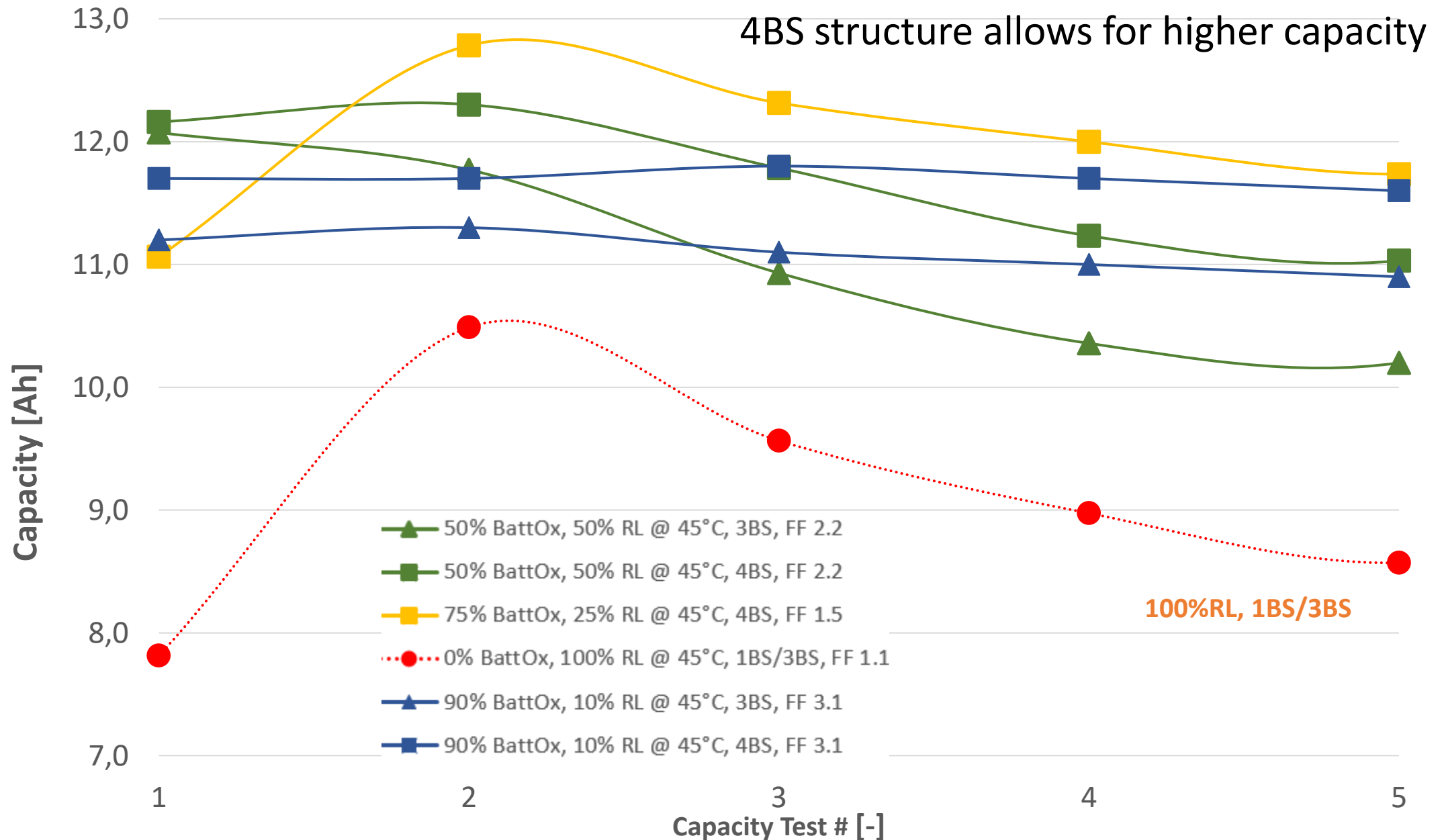
PENOX Negative Plate Potential in Formation



RHE = Reversible hydrogen electrode
Reference potential for the negative electrode

- More **RL** results in less „stress“ for the negative electrode.
- A better balanced formation.

PENOX C5 Capacities (with RL+ tested @25°C)

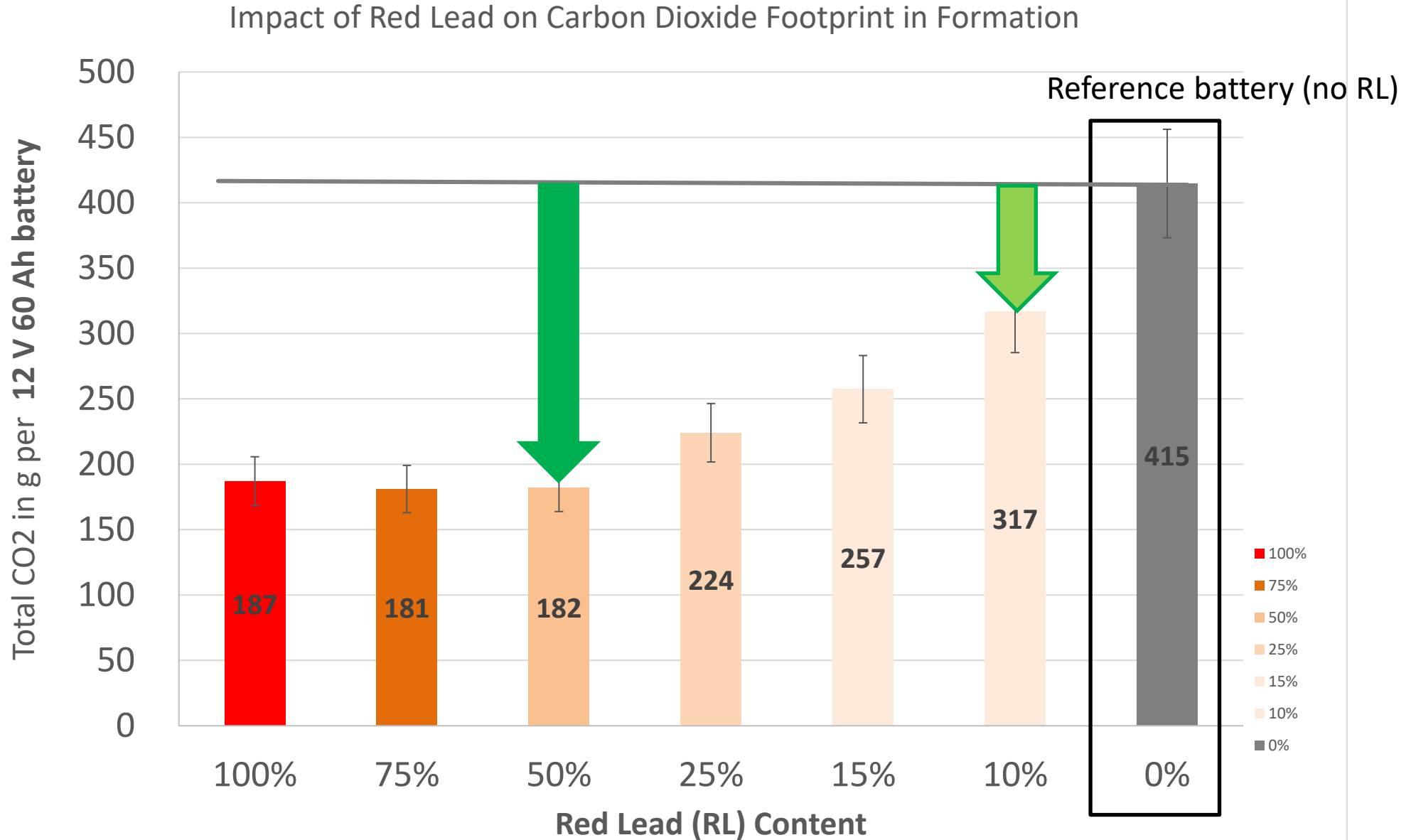


Formation of the **reference cells (only grey lead oxide)** require a formation factor of about **3.7**

Formation of the **reference cells (2V)** require about **420 to 500 Ah per kg** of PAM

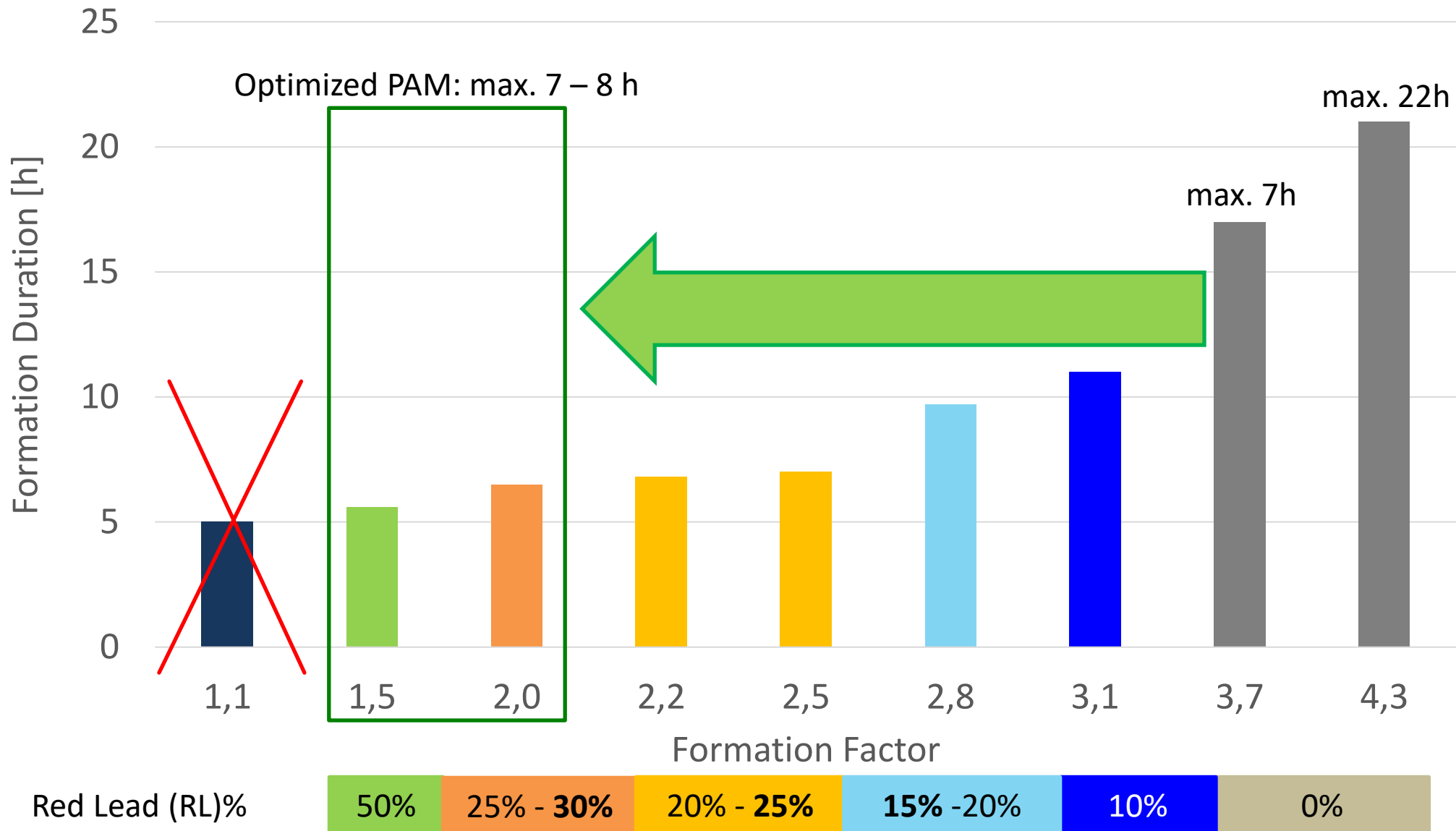
- **Red Lead** allows to reduce the formation energy significantly
 - The effect of **RL addition is not linear** and there is an economical optimum for the RL content
 - **100% RL content** is not allowing for a well developed 4BS structure
 - **50% RL content** allows to reduce the formation factor from 3.1 to **1.5** - a reduction by about **50%**
 - **25% RL** content allows to reduce the formation factor from 3.1 to **2** - a reduction by about **35%**
- Depending on the relative impact of the electricity costs and the value of process time reduction, there is a specific optimum for the RL and **RL+** content.

Impact of Formation Efficiency on CO2 Emissions



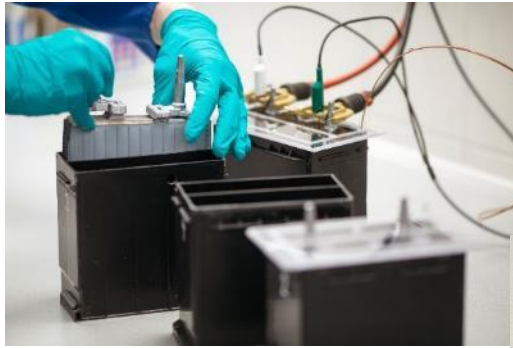
(CO2 emission data is based on [Brazilian energy mix with 120 g CO2 per kWh](#))

Formation Duration per Formation Factor (PENOX – flooded LA Technology)



Red Lead Industrial Grade and **especially RL+** allows for:

- Formation energy **reduced by up to 50% vs. using 100% grey oxide**
- Formation time reduced – depending on the battery technology **by up to 50%**
- **AGM technology has a significant benefit from even small RL content, e.g. 10 w.%**
- **RL+** content can be as low as 10 w.% to achieve a tetrabasic (4BS) structure
- **RL+** allows for higher mass utilisation – higher capacity with same active mass
- **RL+** can be mixed with normal red lead (RL), if higher content of RL is beneficial
- Carbon dioxide foot print is reduced by a more efficient formation:
 - The emission reduction is depending on the carbon dioxide foot print of the electricity generation
 - *In Brazil with about 120 g CO₂ per kWh still a reduction from about 400 g to 200 g for a 12 V 60 Ah battery can be achieved!*



Thank you for your kind interest!

	Requisitos técnicos da EFB 24.02.2022 – V2.0
---	---

Requisitos básicos para
o projeto de um
Bateria EFB

PENOX GmbH
Departamento de I+D
Alemanha

	Technical Guideline 08.08.2023 – V2
---	--

Minimum and Basic Requirements
Addressed to an AGM Design for
Automotive- and UPS-Batteries

PENOX GmbH
R+D Department

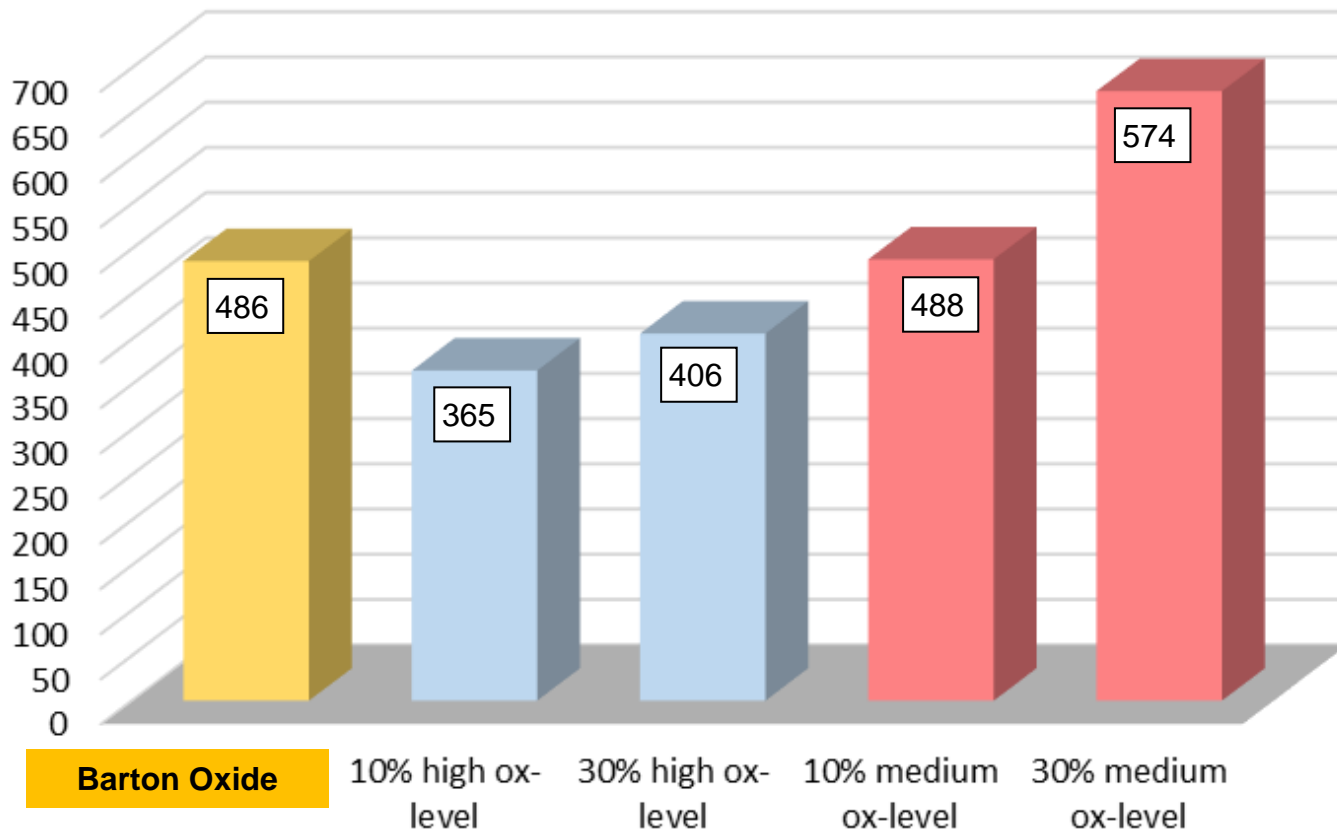
PENOX is supporting customer development activities – Manuscript available on „Basic EFB Design“
[NEW Script on AGM Technology and basic consideration in 08/2023 – for FENIBAT 2023](#)

Appendix

- Slides for discussion -

PENOX Impact of AGM Grade RL on Cycle life*

Red Lead Comparison 17.5% DoD @ 50% SoC

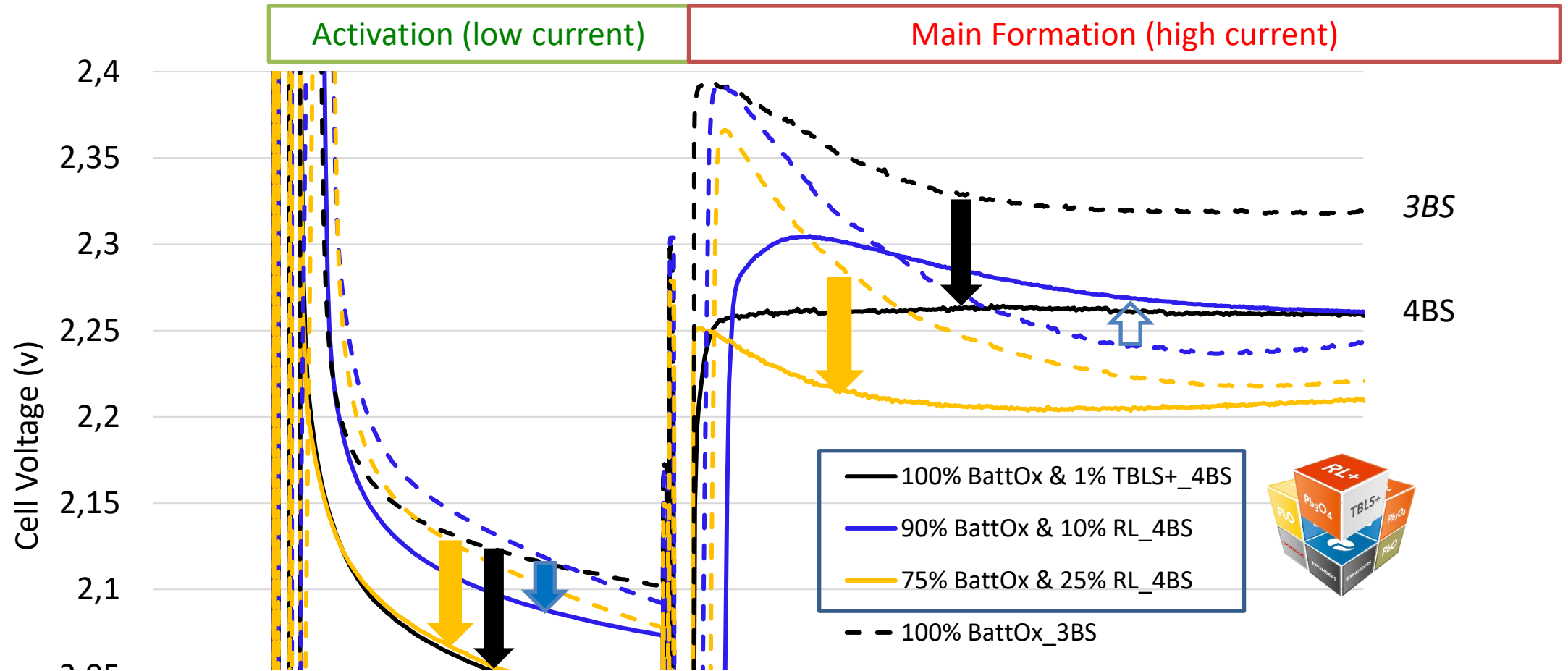


- RL can be highly oxidized, such material is often used in Asia (called “HD” grade)
- RL with lower oxidation is a coarser powder and has a beneficial effect on cycle life
- This effect is eg. seen in a 17.5% DoD test using PENOX AGM grade RL

*18th ELBC, Ian Klein et al.

Grades	Pb ₃ O ₄ [%]	PbO ₂ [%]	β-PbO (residual) [%]	Acid Absorption ¹ [mg acid/g oxide]	D50 ² [micron]
HD grade RL	>96	>33.5	<4	>170	<2
AGM grade RL	77.4 - 86	28 - 30	14 – 22.6	140 - 180	4.5 – 5.5

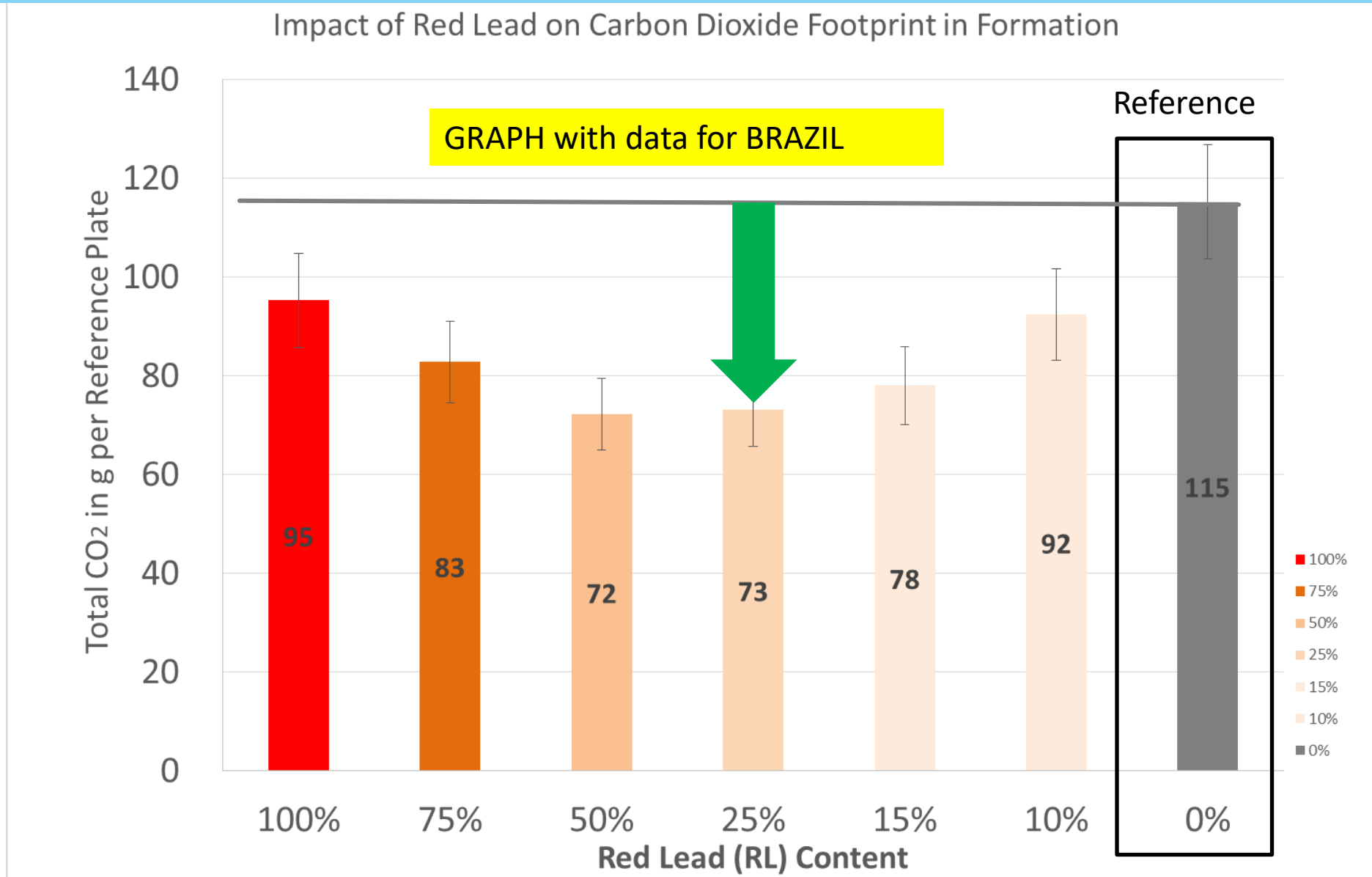
- **Conductivity of the active mass during formation**
 - Cured active masses have a high internal resistance – **RL is increasing the initial conductivity**
- **Current density during a formation step**
 - High current density are impacting both polarities – we need to remember the negative electrode
 - Negative electrodes have a lower surface area with respect to the positive electrode
- **Electrolyte density within the electrode and mass transport**
 - Mass transport is a relevant process during formation
 - Solubility is controlled by local electrolyte density within the active masses
 - Therefore, the structure and porosity of the electrodes are crucial
- **Bulk electrolyte density**
 - Bulk density controls the mass transport of sulfuric acid (generated) within the double-layer and the electrolyte reservoir
- **Temperature of the electrodes**
 - Kinetics are strongly depending on temperature



4BS structure (based on RL+ or TBLS+®) results in lower cell voltage during formation => higher formation energy efficiency in terms of Wh per kg of AM

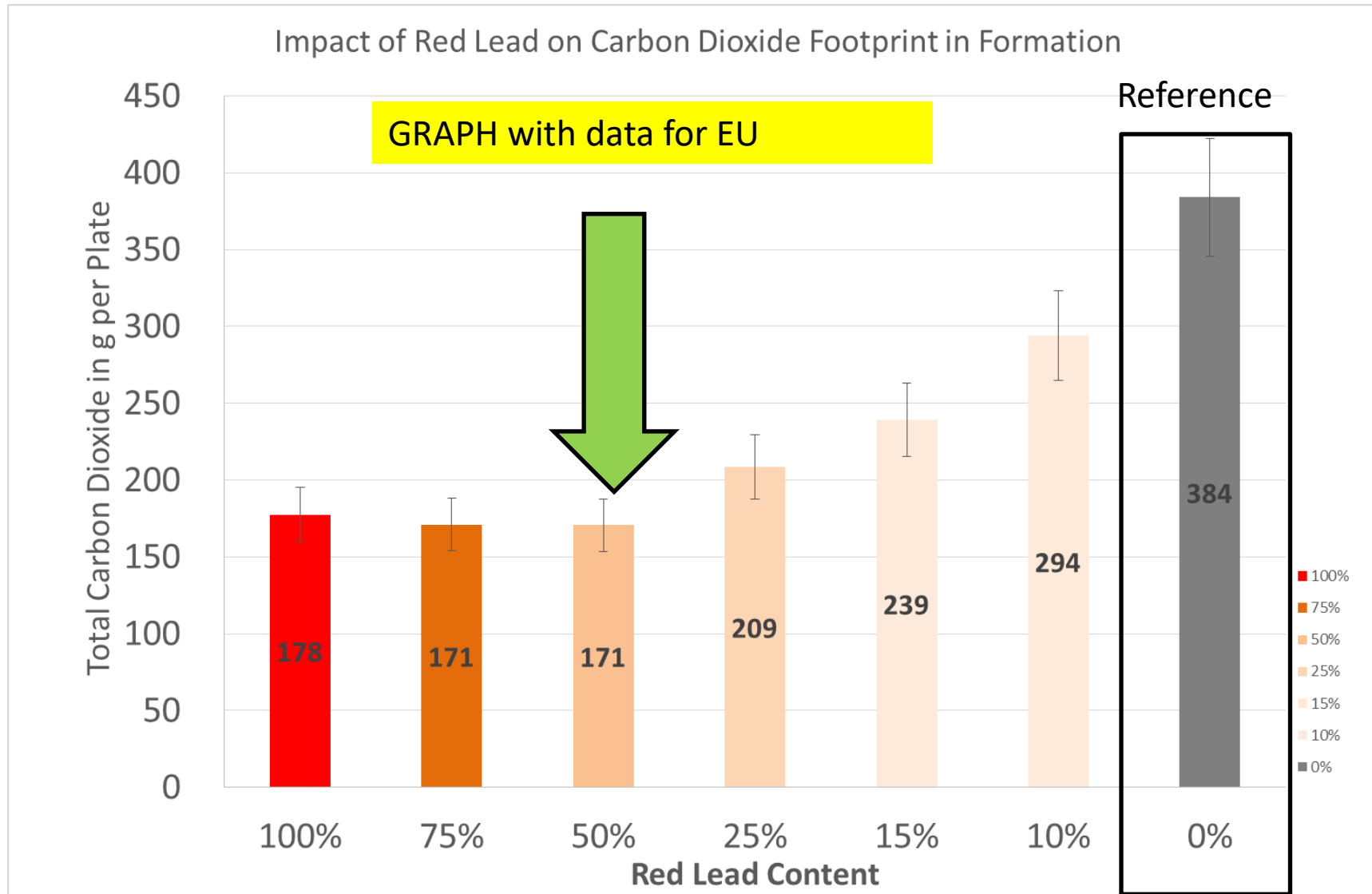
This effect is higher for higher currents used in a formation step!

Impact of Formation Efficiency on CO2 Emissions



(CO2 emission data is based on [Brazilian energy mix with 120 g CO2 per kWh of electricity](#))

Impact of Formation Efficiency on Carbon Dioxide Emissions



(CO2 emission data is based on EU energy mix with 400 g CO2 per kWh of electricity)